

Empirical Model of Recovery Response of Copper Sulphide Circuit at Kansanshi Mine

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Geometallurgical models are a strategic tool used primarily in planning, diagnosis and process optimisation. This paper discusses the development of a predictive model for the flotation recovery of the Kansanshi concentrator in Zambia as a function of key operational parameters. Daily data from the circuit processing the copper sulphide ore for milling and flotation were analysed. These data, recorded over a period of one year of production, were collected from diverse sensors measuring semi-autogenous milling and flotation parameters. Upon performing the relevant statistical analysis, copper head grade, acid insoluble and acid soluble copper, SAG mill throughput, ball mill load, and tonnage of feed material to the SAG mill of size -125 +63 mm were identified to contribute to the prediction power of the proposed empirical model by as much as 90%. Finally, a proposal was made for the development of a simulation model under MODSIM®, a flexible tool for mineral processing applications. This was to test the limitations of the empirical model for future refinement.

INTRODUCTION

Kansanshi is the largest copper mine in Africa and the world's eighth largest copper producer, with a total of 253 272 tons of copper produced in 2016 (Newall, 2017). It is located approximately 10 km north of Solwezi, the capital and administrative headquarters of the North Western province, Republic of Zambia. The ore deposit consists predominantly of chalcopyrite and malachite with variable amounts of chalcocite, bornite, chrysocolla and azurite. Because of the varying proportions of sulphide and oxide copper minerals, the ore is classified into three distinct categories: sulphide, mixed, and oxide ores. As such, three separate processing circuits are used to mill the ore down to a standard targeted grind size of 80% passing 150 µm before froth flotation and leaching.

A lot of research and development has been done to improve the performance of the sulphide ore circuit at Kansanshi. And despite the research effort and subsequent operation, the sulphide ore circuit did not attain the target recovery and grade for 2016, primarily because of the complexity of the ore body.

The constant drive to achieving the set production target of recovery and concentration grade after froth flotation has hence motivated the development of a tool for the prediction of recovery. The anticipated benefit is not only to enable the plant to apply corrective actions when needed, but also to make a tool available for the quick assessment of the performance of the plant. For that, data spanning June 2016 to May 2017 were analysed, cleaned-up and curve-fitted to an empirical model. In doing so, key parameters were determined and calibrate to represent the behaviour of the plant.

KANSANSHI SULPHIDE ORE CIRCUIT

The processing facility linked to the Kansanshi mine entails three separate circuits for three distinct run-of-mine ore feeds: sulphide ore, mixed ores, and oxide ores. The three circuits run in parallel, with each comprising of a dedicated crushing, milling and flotation circuit. The present research work focuses on the sulphide ore circuit.

The sulphide ore circuit at the Kansanshi mine processed an average of 35 000 dry tons per day between 1st June 2016 and 31st May 2017. The run-of-mine sulphide ore undergoes a two-stage primary and secondary crushing in open circuit. The material is then sent to a classic Semi-Autogenous – Ball mill – Crusher circuit, also known as an SABC design. From a processing point of view, the product from the comminution section is sent for froth flotation organised in two stages: roughing in 6 × 300 m³ cells, and cleaning in 8 × 30 m³ cells. Relevant specifications of the comminution equipment are listed in Table I.

Table I: Specifications of the comminution equipment used in the sulphide ore circuit, Kansanshi.

Primary crusher	Gyratory crusher Model: Metso 54 – 75 Available power: 450 kW Open side setting: 125–200 mm Closed side setting: 90–120 mm
Secondary crusher	Nordberg MP800 Available power: 600 kW Closed side setting: 40–55 mm
Pebble crusher	Terex Cedarapids MVP 450 Available power: 315 kW Closed side setting: 12 mm
Semi-autogenous mill	Internal diameter: 9.75 m Internal belly length: 6.10 m Centre line length: 8.9 m Available power: 11.6 MW Grate discharge design Speed: 75% of critical (VSD) Ball filling: 19% Top-up ball size: 125 mm 80% passing feed size: 125 mm
Ball mill	Internal diameter: 6.10 m Internal belly length: 9.30 m Centre line length: 10.5 m Available power: 5.8 MW Overflow discharge design Speed: 75% of critical Ball filling: 28% Top-up ball size: 50 mm Average Bond Work index: 9.2 kWh/t

METHODOLOGY

The primary objective of a processing plant is to produce good quality concentrates at the highest levels of recovery and throughput and at the lowest operation costs. The attainment of this objective resides in the quality of the ore feed, the geometry, configuration and operating conditions of all the processing units involved and, most importantly, an accurate knowledge and understanding of the circuit behaviour.

Concentrators generally experience variable metallurgical recovery, to the extent that it has become common practice to attempt to model the behaviour of the concentrator as a function of key operating parameters. To do that, in-house databases can be resorted to with the data coming for example in the form of historical operational performance data of the plant, planned surveys, geo-metallurgical data, and ore characteristics. The work by Compan *et al.* (2015) exemplifies this with a regression model proposed for the Chuquicamata plant treating by milling and flotation a copper sulphide ore.

In this section, an attempt to produce an empirical model similar to that of the Chuquicamata plant was made. To this end, key input parameters that will make up the model were identified before the structure of the model was proposed. The data were pre-processed so that curve-fitting by non-linear regression was performed. This was to determine the values of the parameters of the model and calibrate them to the Kansanshi operation.

Identification of Key Input Parameters for Model Building

The Kansanshi plant is fitted with a wide array of sensors for monitoring its general performance. For example, a camera-based system is used to measure the particle size distribution of the feed to the SAG mill and weightometers are installed on the belt conveyors of all major units to get a reading of the mass flow. Flowmeter, densitometer, pressure readers and level sensors are also used in the flotation section. Figure 1 illustrates a typical signal from a weightometer measuring the SAG mill load.

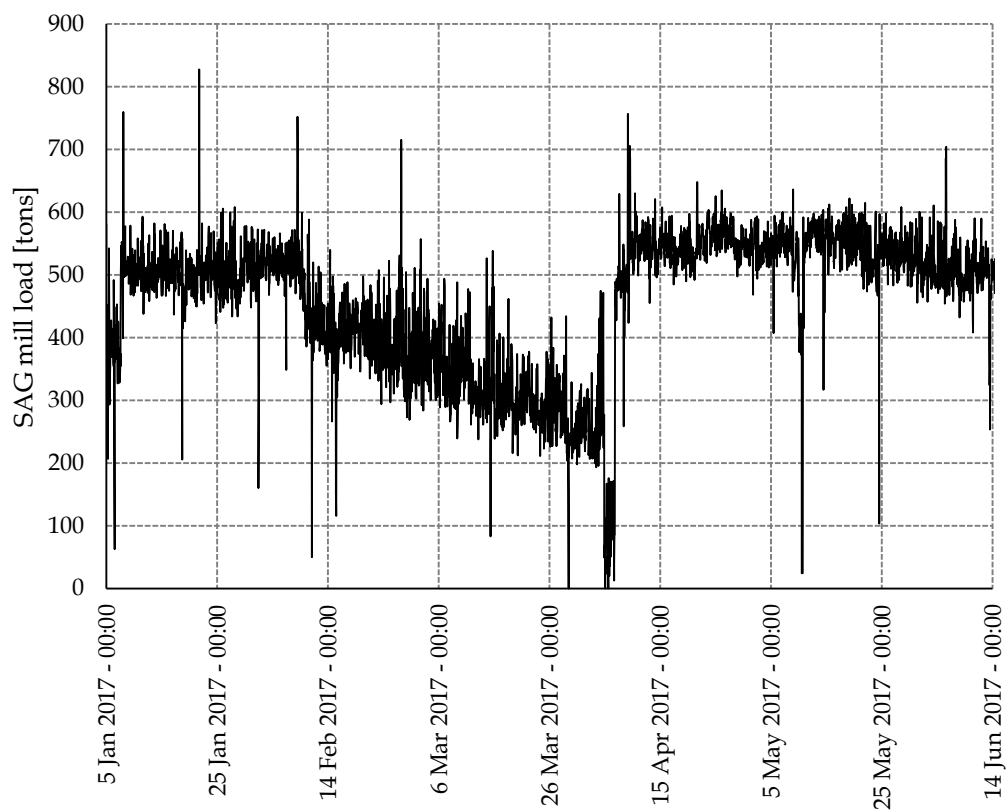


Figure 1: Example of signal from the SAG mill load weightometer between 05 January and 14 June 2017.

Overall, 29 signals are collected from the SABC section and 49 signals comes from the flotation section. It becomes clear that, to produce a useful and flexible model of the plant, the number of input parameters should be cut down to a reasonable minimum.

King (2012) described in a comprehensive manner the most important phenomenological models that can be used in the description of a wide variety of mineral processing units. These units include SAG mills, ball mills, hydrocyclones and flotation since these are relevant to Kansanshi. A critical review of

the models applicable to each unit reveals that, of the 78 signals streamed from the Kansanshi sulphide ore circuit, 11 signals may be used to model the performance of the plant with reasonable accuracy. The list of these 11 parameters identified is given in Table II.

Table II: Input parameters of the recovery response model of the sulphide ore circuit, Kansanshi.

Parameter	Measuring instrument	Mathematical symbol [units]
SAG mill throughput	Weightometer	Q [t/h]
–22 mm feed size fraction	Camera	W_1 [t]
–63 +22 mm feed size fraction	Camera	W_2 [t]
–152 +63 mm feed size fraction	Camera	W_3 [t]
Ball mill load	Set point	J [t]
Flotation feed flowrate	Flowmeter	F [m ³ /h]
Flotation feed density	Densitometer	C_w [% solids]
Flotation feed grade	Camera	$\overline{Cu}$ [% Cu]
Bubble velocity	Camera	v [mm/s]
Air flowrate	Flowmeter	a [m ³ /h]
Froth level	Level sensor	f [mm]

By consulting King (2012), the choice of the key parameters above was also supported by the following references: Austin *et al.* (1984), Compan *et al.* (2015), Hu (2014), Klimpel (1995), Napier-Munn *et al.* (1996); Pease *et al.* (2006) and Yahyaei *et al.* (2014).

Development of Empirical Model of Kansanshi Sulphide Ore Circuit

The work by Compan *et al.* (2015) was mentioned earlier to serve as the basis for the development of a regression model for use in determining the copper recovery of the Kansanshi sulphide ore circuit. This is because the aforementioned work was done on the Chuquicamata plant processing a sulphide copper containing mineralogical species such as chalcocite, chalcopyrite and molybdenite also found in the Kansanshi sulphide ore type. The following model was proposed for the Chuquicamata (Compan *et al.*, 2015):

$$R_{Cu} = -264.74 + 31.243 \left[1 - \exp \left(-\frac{\overline{Cu} - 0.22}{0.11} \right) \right] + 12.24 \overline{Fe} - 6.7 \overline{Fe}^2 - 2.88 \overline{CuS} + 0.6 \overline{Mo}^2 + 2.94 \overline{Cp}^2 - 0.92 \overline{Dg}^2 - 15.01 W_i^2 + 4.04 \overline{P80}^2 \quad [1]$$

where R_{Cu} is the final copper recovery after flotation; $\overline{Cu}$ is the copper feed grade; $\overline{Fe}$ and $\overline{CuS}$ are, respectively, the iron and copper sulphide feed grades to the plant; $\overline{Mo}$, $\overline{Cp}$, and $\overline{Dg}$, are the molybdenite, chalcopyrite and digenite grades in the ore feed; and W_i and $\overline{P80}$ are the work index and product size of the ore after milling.

A look at Equation [1] shows that the majority of input parameters in the Chuquicamata response function are grades of some mineral species making up the ore feed. The parameters and the additional work index W_i and product size $\overline{P80}$ are all physical properties of the ore. No parameter relating to operating conditions of milling and flotation is included although the model should be representing the two processes. This is probably ascribed to the fact that the parameters in Equation [1] are amongst those monitored on the plant. The Kansanshi case is different in the sense that a wide range of parameters is measured around the plant but none is to do with ore properties (see Table II).

The general problem with empirical models is that they are developed based on available information. This, in a sense, forces one to overlook critical parameters in building the model; hence, their limitation. The advantage, however, this type of model offers is primarily their simple structure, flexible use and quick manipulation when estimates are needed, amongst others.

This brings us to discuss the structure of the empirical model of recovery response proposed for the Kansanshi copper sulphide ore circuit. The following equation was proposed for testing on the Kansanshi data at our disposal:

$$R_{Cu} = C_0 + C_1 Q J + C_2 W_1^{1.3} + C_3 W_2^{2.5} + C_4 W_3^{3.7} + C_5 v^{-0.5} + C_6 a^{2.8} f^{8.6} + C_7 [\exp(-C_w)] \left[1 - \exp\left(-\frac{\overline{Cu} - C_8}{C_9}\right) \right] \quad [2]$$

where C_0 to C_9 are the model coefficients that needed to be determined by the nonlinear regression of the Kansanshi data collected between June 2016 and May 2017. Thirty percent of this data was used in the calculation of the model coefficients above while the remaining 70% served to assess the predictive ability of the model proposed in Equation [2]. The outcome of this endeavour is presented in the next section.

RESULTS AND DISCUSSION

The results of the regression analysis are presented in this section. The adequacy of the model and that of the regressed coefficients are also discussed. A proposal is made for a simple model based on the contribution of each parameter.

As a starting point, Equation [2] was curve-fitted against the copper recovery data in the least squares sense. This means that initial guesses were allocated to the coefficients C_0 to C_9 ; then, the sum of squared differences between the theoretical and actual copper recovery values was calculated. A computer algorithm was finally involved to iteratively adjust the values of the coefficients until the sum of squared differences converged to a global minimum. Table III summarizes this result, with each coefficient value allocated its 95% confidence interval.

Table III: Values of coefficients for recovery response model of sulphide ore circuit, Kansanshi.

Coefficient	Regressed value	95% confidence interval
C_0	70.4	± 12.1
C_1	328×10^{-8}	$\pm 14 \times 10^{-8}$
C_2	-223×10^{-4}	$\pm 87 \times 10^{-4}$
C_3	141×10^{-5}	$\pm 74 \times 10^{-5}$
C_4	0.13	± 0.02
C_5	-0.056	± 0.032
C_6	157×10^{-12}	$\pm 61 \times 10^{-12}$
C_7	12.6	± 0.2
C_8	0.78	± 0.09
C_9	0.25	± 0.03

Figure 2 illustrates the results of the curve-fitting performed on the recovery data spanning June 2016 to September 2016. The theoretical and actual time-series curves are superimposed for the time duration of interest.

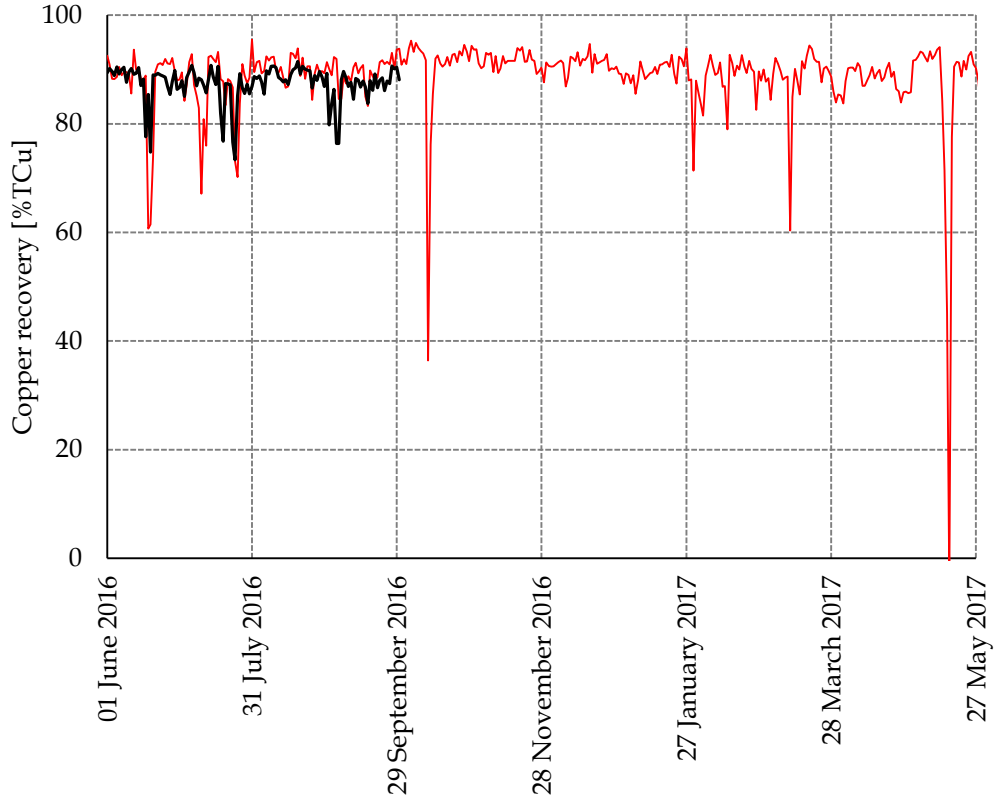


Figure 2: Time-series plots of the actual (in red) and the curve-fitted (in black) copper recovery at the Kansanshi copper sulphide ore circuit between 01 June 2016 and 30 September 2016.

Based on the regressed coefficient values in Table III as well as their respective confidence interval at a 95% significance level, it was decided to set the following coefficients at zero: C_2 , C_3 , C_5 and C_6 . The decision to eliminate these coefficients was primarily based on their poor level of accuracy with respect to their average regressed values. In doing so, Equation [2] was simplified and reduced to the following form:

$$R_{Cu} = C_0 + C_1 Q J + C_4 W_3^k + C_7 \left[1 - \exp\left(-\frac{\overline{Cu} - C_8}{C_9}\right) \right]. \quad [3]$$

It should be noted in Equation [2] that input parameter C_w is now absorbed into coefficient C_7 . This is because this particular parameter representing the flotation feed density (see Table II) did not vary significantly for the year-worth of operation data collected. Besides, for the sake of simplicity, the lower the number of input parameters, the better for the model. This, of course, needs to be balanced with an acceptable level of accuracy within the accuracy of the various measuring and monitoring used at the plant. That is why, a new exponent parameter k was introduced around parameter W_3 to add flexibility to the curve-fitting procedure.

With a simplified definition of the empirical model of recovery response of the Kansanshi copper sulphide circuit, a new regression analysis was initiated. This time, seven coefficients were regressed and their uncertainties still calculated at a significance level of 95%. The outputs from the curve-fitting algorithm are reported in Table IV.

Table IV: Values of coefficients for simplified recovery response model of sulphide ore circuit, Kansanshi.

Coefficient	Regressed value	95% confidence interval
C_0	76.1	± 8.6
C_1	106×10^{-7}	$\pm 9 \times 10^{-7}$
C_4	0.911	± 12
C_7	21.213	± 0.007
C_8	0.076	± 0.005
C_9	0.36	± 0.03
k	0.5323	± 0.0034

It can be noted that the parameters in Table IV are more accurately predicted than those in Table III based their errors at 95% significance level. In addition to this, when validated again the data between 1 October 2016 and 31 May 2017, a striking similarity is evident, as shown in Figure 3. To confirm this observation, the coefficient of determination R^2 of Equation [3] was calculated. This statistic was found to be $R^2 = 0.694$, meaning that 69.4 % of the data considered can be explained by Equation [3]. Compared with a coefficient of determination $R^2 = 0.557$ for Equation [2], it is clear that Equation [3] is preferable, especially considering its simple format.

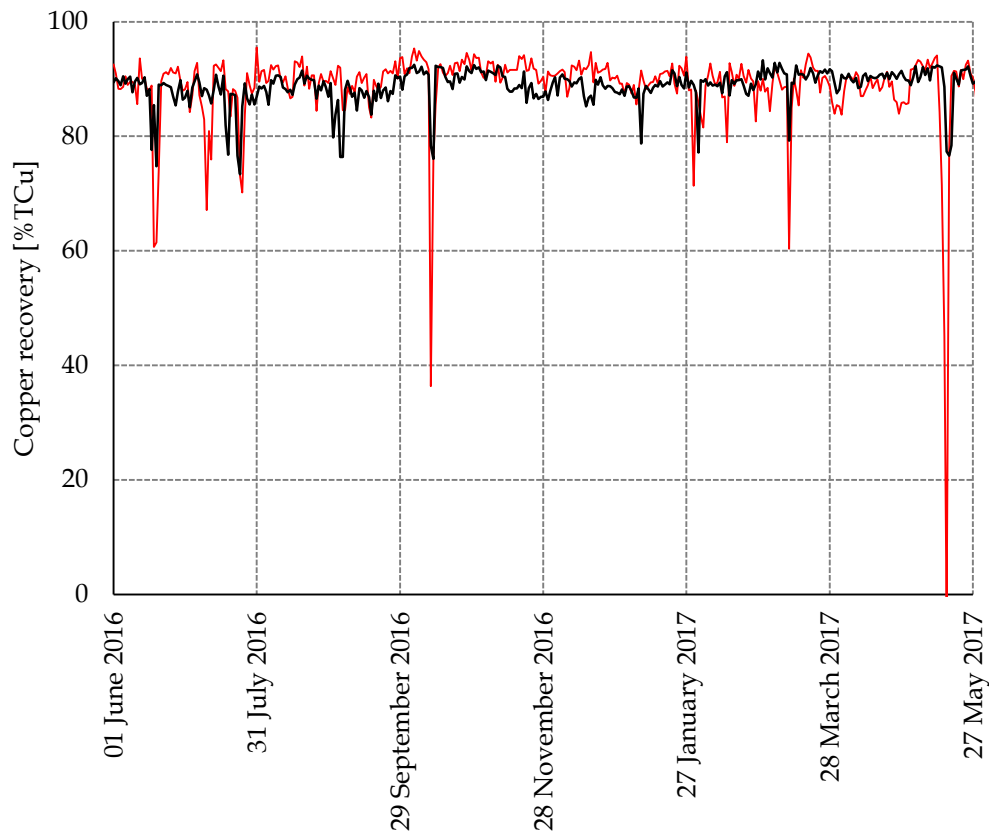


Figure 3: Actual (in red) and predicted (in black) recoveries of Kansanshi copper sulphide ore circuit between 1 June 2016 and 31 May 2017. Prediction estimates were computed using Equation [3] and Table IV.

It is clear that some long negative peaks are not well reproduced by the model; however, the general trend, including the slight cyclical nature of the actual copper recovery data, is followed to an acceptable extent. The other thing of concern is that the coefficient of determination may require further improvement. For that to be done, relevant operating parameters perhaps not yet available or not shortlisted in Table II should be explored for inclusion into the model.

To further improve on the predictive ability, the inclusion of the percent acid soluble copper ($AsCu$), the ratio of acid insoluble copper to total copper ($AiCu/TCu$) and the difference between total copper

(TCu) and total copper mean for the dataset (TCu) into the empirical model was explored. In doing so, Equation [3] was modified to the following form:

$$R_{Cu} = C_0 + C_1 Q J + C_4 W_3^k + C_7 \left[1 - \exp\left(-\frac{TCu - C_8}{C_9}\right) \right] + C_{10} AsCu + C_{11} \frac{AiCu}{TCu} + C_{12} (TCu - TCuMean) \quad [4]$$

A new regression analysis was performed based on Equation [4]. This time, 10 coefficients were regressed and their uncertainties still calculated at a significance level of 95 %. The outputs from the curve-fitting algorithm are reported in Table V.

Table V: Values of the coefficients to the alternative recovery response model in Equation [4].

Coefficient	Regressed value
C_0	27.4
C_1	1.301×10^{-5}
C_4	3.550
C_7	1.883
C_8	1.521
C_9	0.11
C_{10}	62.87
C_{11}	45.1
C_{12}	6.526
k	0.2896

The result of this analysis reported in Table V was also validated against the data between 01 June 2016 and 31 May 2017. Here, a coefficient of determination $R^2 = 0.904$ was noted for Equation [4]. A parity plot in Figure 4 is provided to support this with data points representing weekly average recoveries calculated over the period running from 01 June 2016 to 31 May 2017.

The improved coefficient of determination $R^2 = 0.904$ simply means that Equation [4] describes 90.4 % of the data well with the remaining 9.6 % being attributed to uncertainties inherent to the plant data collected as well as the structure of the model. However, an improvement is noted from $R^2 = 0.694$ for Equation [3] with a more complex structure for Equation [4].

Finally, empirical models are generally useful and simple to use while their format is based on the experience of the researchers involved. One shortcoming though is that they need constant refinement and calibration. Therefore, they should be used with caution beyond the average operating conditions under which they were developed. More realistic models are needed for application in wider operating ranges. Phenomenological models built around the population balance model (Austin *et al.*, 1984; King, 2012) are good examples of realistic models of mineral processing operations. That is why, further work is necessary to produce such type of a model for the Kansanshi copper sulphide ore circuit. A simplified version of the anticipated model may then serve the purpose better than Equations [3] and [4] in a wider operating range. The drawback may be the complex format of this type of model and the need to define an increased number of input parameters. For as long as the phenomenological model or its simplified version are not available, the proposed empirical model should be used.

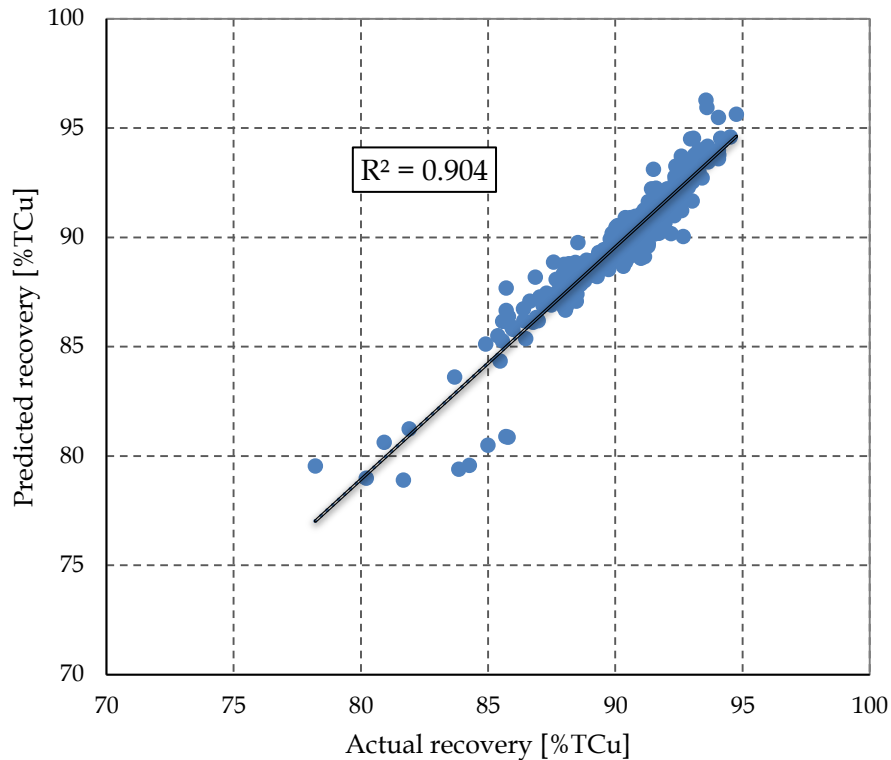


Figure 4: Parity plot showing the adequacy of Equation [4] as the empirical model of recovery response of the copper sulphide circuit at the Kansanshi concentrator

CONCLUSION

The objective of this research was to develop a predictive model for copper recovery for the Kansanshi copper sulphide ore circuit. All available data collected online from the operation were reviewed to shortlist those believed to be important input parameters to the model. In addition, the literature was studied to determine an initial form of the empirical model.

The model building ensued once only 11 operating parameters of the circuit were retained; the information from the signals corresponding to each parameter was then extracted for the period from 1 June 2016 to 31 May 2017. This time-series data were curve-fitted using the empirical model initially proposed and the relevant statistics were produced in the process. From the statistics, it was clear that some regressed fitting coefficients added little to the accuracy of the model. These were eliminated and, consequently, the empirical model took a simplified format that only included seven fitting coefficients and four input parameters. The input parameters are the copper head grade at the flotation section, the SAG mill throughput, the ball mill load, and the tonnage of feed material to the SAG mill of size $-152 +63$ mm. The regression analysis revealed that the simplified empirical model accounts for approximately 90% of the copper recovery data. This means that there is room for improvement on the model; this may come in the form of the inclusion of parameters not currently measured or those that were not shortlisted in the development of the initial model. Despite some limitations, the model has the potential to serve the purpose of quickly estimating the expected recovery under given operating conditions. This timely information may help make sense of the actual recovery and identify avenues for corrective action guided by production targets.

Finally, work is currently underway aimed at developing a model of the behaviour of the Kansanshi copper sulphide ore circuit. This computer model will be based on a more theoretical description of unit processes using MODSIM®, a specialised module simulator for mineral processing operations. This will become an additional, yet more comprehensive, tool to the process engineers for efficient operation of the plant.

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