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# **Prospects for value addition in copper in the emerging Kalahari Copper Belt of Botswana**

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# Synopsis

The Kalahari Copper Belt (KCB), which stretches for about a 1000 km in northwestern Botswana, is emerging as a potential host to new copper and silver mining projects. Current resources are estimated at about 472 Mt at grades ranging from 0.85% to 2.2% copper and 11 to 50 g/t silver. In this paper, we constructed a discounted cash flow financial model of an Isasmelt technology copper smelter and sulphuric acid complex, and then used the model to determine the minimum economic size of a copper smelter and its attendant sulphuric acid plant in the KCB, whether current and future production of copper concentrates would provide sufficient feed leading to satisfactory project economics for the smelter, and the level of imports of copper concentrates, if any, that would be required to ensure that the smelter operates at full capacity. The study concluded that the minimum economic size of the smelter would be 485 kt per annum and that the projected tonnages of local copper concentrates would, on their own, fail to provide enough feed to the smelter. We recommend further work to more accurately define the likely production of copper concentrates from the KCB; the possibility of imports of copper concentrates; taxing the smelter at rates for manufacturing, which are currently 15% as opposed to the company tax rate of 22%; and the possibility of negotiating lower electricity tariffs as this would lead to improved project economics for the smelter and sulphuric acid complex.

#### Keywords

copper value chain, Kalahari Copper Belt, project economics, copper smelter.

# Introduction

The Kalahari Copper Belt (KCB) stretches for about 1000 km from south of Maun in Botswana through Ghanzi and into Namibia The estimated copper resources reported on the company websites of Khoemacau Copper mine (Cupric Canyon, 2018) and Tshukudu Metals' T3 project (Mod Resources, 2018) for their exploration projects amount to some 472 Mt at grades varying from 0.852.2% copper and 11–50 g/t silver. Two of the projects in the KCB with potential for developing into producing mines are Cupric Canyon's Khoemacau Zone 5 and Tshukudu Metals' T3 project. The Khoemacau Zone 5 project, currently at the mine development stage, has resources estimated at 100.3 Mt at 1.95% copper and 20 g/t silver. The Tshukudu Metals T3 project is at the full feasibility study stage and has resources of 60 Mt at 0.98% copper and 14 g/t silver. Cradle Arc plc, a majority owner of Mowana Copper Mine, some 100 km west of Francistown, reports on its website that the mine has copper resources of 72 Mt at 1.5% copper and is currently producing about 12 000 t of copper in concentrate per annum (Cradle Arc plc, 2018). The two proposed projects are reported to have robust project economics with C1 cash costs net of silver credits of US\$1.00 per pound for Khoemacau Zone 5 and US\$1.22 per pound for the T3 project.

The mineralogy of the copper sulphide ores in the KCB consists of chalcocite, chalcopyrite, and bornite. The Khoemacau project will initially use the Boseto Copper processing plant, which is under care and maintenance, to produce copper and silver in concentrate for sale to regional and international copper smelters and refiners. The T3 project prefeasibility study indicates that while the concentrate to be produced will be relatively free of deleterious elements, there will be further investigations at the full feasibility study phase to lower the lead, arsenic, and bismuth contents to below smelter penalty levels (Mod Resources, 2018).

# Candidate smelting technologies

Copper smelting technologies are well established, and the choice of technology is based mainly on capital and operating costs as well as the efficient capture of the sulphur dioxide gas to produce

sulphuric acid. The global trend in growth in new copper smelter capacity has been based on two technologies - Outotec flash smelting, which includes flash smelting, flash converting, and direct-to-blister flash smelting; and top submerged lance or TSL, which includes Ausmelt and ISASMELT (Kojo, Scheidema, and Reuter, 2015). In the Southern African region, recent installation of copper smelters with sulphuric acid plants include the Mufulira smelter upgrade project in Zambia, where an ISASMELT furnace replaced an electric furnace in 2006, resulting in about a 40% reduction in operating costs (Barlows et al., 2012) and the Kansanshi smelter and sulphuric acid complex in 2015 (First Quantum Minerals Ltd, 2012). The advantages that have been cited by mines in Zambia for the selection of TSL over flash smelting technology include a smaller footprint, lower capital and operating costs, and ease of operation (Roos and de Vries, 2005; Barlows et al., 2012).

The process flow diagram for an ISASMELT copper smelter and acid plant is shown in Figure 1. In summary, the smelter would treat copper concentrates to produce copper anodes for refining in regional or overseas refineries to produce cathode copper and silver. The off-gas from the smelting furnace would be used to produce sulphuric acid, which has application in copper refining as well as the manufacture of fertilizers.

# Value addition drivers for copper

Copper is traded internationally as concentrate, matte, blister, anode, or cathode copper. The factors that influence the level of value addition for a copper deposit are profitability, capacity utilization of the beneficiation facility, environmental compliance costs, proximity to semi-fabricators and downstream manufacturers of copper based products, supply and demand, as well as copper price volatility. The main factor that influences the decision to either sell concentrate or smelt on site is profitability; this is because mining provides the highest returns on investment as compared to smelting and refining. Low capacity utilization of existing smelters puts downward pressure on the treatment and refining charges, thus improving the net smelter returns to mining companies. On the other hand, environmental compliance costs for sulphur dioxide abatement are not only high, but would also require the construction of a sulphuric acid plant and tend to discourage the establishment of smelting and refining facilities on mining sites (World Bank, 2012). The location of copper concentrate smelting and refinery complexes is largely influenced by the existence, in close proximity, of semifabricators and other downstream manufacturers of copper-based products (World Bank, 2012). It is for this reason that most copper smelters and refiners are located in major industrialized regions of the world, such as in Asia (mainly China, Japan, South Korea, and South East Asia), Europe, and the USA (World Bank, 2011). A major technical advantage of this is that mill scrap generated during fabrication and other downstream processes can be recycled in the smelters.

The current global supply deficit for refined copper is likely to widen due to a variety of factors that may interrupt supply (Lee and Shin, 2018). For instance, the copper project pipeline fell by about 50% between 2011 and 2017 and there are no copper mining projects currently nearing production (Glasenberg, 2018). Other long-term supply challenges include the decline in production levels due to a variety of reasons, chief among which are the ageing of current major producing mines, declining grades, and closure at end of mine life (Glasenberg, 2018; Lee and Shin, 2018). The demand for copper is dominated by China, which is the world's largest importer of copper in intermediate products (Economic Research Institute, 2017) and in 2016 accounted for just over one-third of global copper smelter production (International Copper Study Group, 2018). It is projected that the supply-demand deficit for China will average some 4.5-5.5 Mt/a over the period 2020 to 2030 (Zhang et al., 2015). The key drivers of future demand for copper include the electric vehicle market, which some analyst project would contribute significantly to global demand. For instance, Lee and Shin 2018) forecast an annual growth rate of 22% until 2030, at which time electric vehicles will make up some 8.2% of global demand for copper, while Glasenberg (2018) anticipates a 30%



Figure 1-Process flow diagram of an ISASMELT copper smelter and acid plant (adapted from Roos and de Vries, 2005)

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market share target for electric vehicles in 2030, resulting in an 18% increase over the 2017 global demand for copper.

Copper prices are fairly stable and are forecast to remain in a narrow trading band over the next five years (Lee and Shin, 2018). For instance, the World Bank forecasts nominal copper prices to be US\$3.14 per pound in 2025, up only slightly from US\$3.08 per pound in 2018, even though a deficit in supply is forecast. This should lessen the market risk faced by any new copper projects in the development pipeline.

Lessons from the Zambian copper sector, which has achieved beneficiation levels up to the production of refined copper, demonstrate that at the appropriate scale, copper beneficiation is profitable in landlocked mining countries. The challenge, it seems, is that of further value addition by way of fabrication and end-user products (Mulunda, Musonda, and Luwaya, 2015). In a related study, the major impediments to Zambia's progression into fabrication and end-user manufacturing were cited as the small size of the domestic and continental market, which is currently serviced by manufacturers in South Africa, and the inefficient transport system to export end-user products to the international markets (World Bank, 2011).

For the policy-maker, the mining sector presents opportunities for downstream economic linkages through mineral beneficiation. There is therefore great interest by policy-makers in Botswana to determine whether the existing and proposed copper and silver mining projects can sustain further beneficiation of copper beyond the production of concentrates, and what policy interventions, if any, would facilitate such activities. The other factors that have to be considered by the policy-maker are the challenges that a copper mine located in the KCB would face in getting its products to market due to the landlocked nature of the country, lack of rail infrastructure for exports of high volumes of concentrates, the attendant long distance to ports, as well as the long distances by sea to smelters in the Far East.

The KCB has huge reserves of copper and silver, and value addition along the copper value chain has the potential to go beyond the production of concentrate. The purpose of this research was to establish whether the projected tonnage of concentrates from projects at advanced stages of exploration and mine development in the KCB would justify the establishment of a custom copper smelter with a sulphuric acid plant.

# Material and methods

The projected local concentrate production, revenues to the smelter in the form of treatment charges, and capital and operating costs of an ISASMELT technology-based smelter were used to develop a desktop financial model that was used to evaluate the likely profitability of a standalone smelter and sulphuric acid complex. This smelter complex could either operate on a full toll smelting basis or as a custom smelter, thus either purchasing concentrates outright or toll smelting for producers in the KCB and the region. A sulphuric acid plant was included in each case to ensure that the project would be environmentally compliant.

In order to develop a discounted cash flow financial model of the smelter and sulphuric acid complex, the data from KCB projects was used as input to the model. The data includes timing and production of concentrate, quality of concentrates, mineralogical composition of the concentrate, treatment charges, labour and power costs, and finally the capital costs of the smelter and sulphuric acid plant. An after-tax desktop financial evaluation of a standalone copper smelter to smelt copper concentrates from mines in the KCB and other parts of the country and (possibly) the region was developed.

# Data

# Concentrate production and timing

Data on planned concentrate production and the likely timing of such concentrates was obtained from the websites of companies involved in exploration for copper in the KCB. Data for concentrate production under two possible scenarios, the base and expansion cases, is presented in Tables I and II respectively.

It is apparent that the approach by the exploration companies is to start the mining projects to demonstrate the robustness of project economics, and then rely on this to raise capital for expanded production. This approach is taken as the most likely scenario regarding the development of the copper mining projects in the KCB. Table II presents the projected concentrate production under this most likely scenario of the expansion case.

# Spot treatment and refining charges

The revenue stream to a copper smelter consists of treatment, refining, and penalty charges (TR/RC plus penalties), metal premiums, free metal, and by-products. These are presented in Table III together with their computation (New Boliden, 2017; Söderström, 2008). Typical net smelter return contract terms

#### Table I

# Estimated production of copper concentrates from Botswana projects under the base case

Year	Production (kt)									
	1	2	3	4	5	6	7	8–13	14	15–25
T3 open pit	0	0	0	70	70	70	70	70	0	0
Zone 5	0	0	140	140	140	140	70	140	140	140
Mowana	62	62	80	62	62	62	62	62	62	0
Total	62	62	220	272	272	272	272	272	202	140
Grades										
% Cu (%)	34	34	39	38	38	38	38	38	38	42
Ag (oz/t)	0	0	198	258	258	258	258	258	216	312
Weighted average grades of total concentrates based on estimated mine production from projects and information on company websites										

#### Table II

# Estimated production of copper concentrates from Botswana projects under the expansion case

	Production (kt)									
Year	1	2	3	4	5	6	7	8–13	14	15–25
T3 open pit	0	0	0	70	70	70	93	93	0	0
Zone 5	0	0	140	140	140	140	70	233	233	233
Mowana	62	62	80	62	62	62	62	62	62	0
Total	62	62	220	272	272	272	295	388	295	233
Grades										
Cu (%)	34	34	39	38	38	38	38	39	40	42
Ag (oz/t)	0	0	198	258	258	258	258	278	246	312
Weighted average grades of total concentrates based on estimated mine production from projects and information on company websites										

#### Table III

#### The revenue stream for a copper smelter producing copper anodes and acid

Variable	Basis (2018)	Computation based on typical NSR terms	Contribution (US\$/ton conc.)					
Treatment charges (US\$/ t conc. with no price participation)	\$90/ton	1.0 DMT × \$78/ton	90.00					
Free copper (% Cu recovery – % payable Cu)	\$6800/ton	(98%-96.75%) × 38% × \$6800/ton	32.30					
Free silver (g/t Ag recovery – g/t payable silver)	\$17/ troy Oz	(98%-90%) × (258-30) g/ton/31.10 g/oz × \$17.0/oz	9.97					
Sulphuric acid (S in conc. estimated at 26.22% and 95% smelter recovery)	\$118.38 FCA site	Tons acid = 26.22% × (98/32) × 95% = 0.763 Value = 0.763 × \$118.36 /ton	90.31					
Metal premium	\$78.50	MP = 38% × 98% × \$78.50 / ton	29.23					
Total smelter plus $H_2SO_4$ plant revenues per dry ton concentrate			\$251.81					
Compiled by the authors based on web sources cited under this section								

Table IV							
The estimated number of employees and annual cost of labour							
Estimated number of workers <sup>a</sup>	Estimated monthly cash earnings for mining (US\$) <sup>b</sup>	Estimated annual cash earnings (US\$)					
600	1710.42	12 315 024					

<sup>a</sup> Based on the Kansanshi copper smelter and sulphuric acid project.

<sup>b</sup> The total monthly cash earnings in the mining and quarrying sector as at September 2017 was BWP 17 666. This is adjusted by a 3% inflation to BWP18 195.98, which is equivalent to US\$1710.42 per month.

Table V								
The annual cost of power								
Electricity (MWh/t anode)ª	Est. Cu anode (t)	Annual MWh consumed	Estimated demand (MW)	Energy charge (US\$/kWh)⁵	Demand charge (US\$/kW)⁵	Totsl est. energy and demand charge (US\$)		
1.39	185 417	257 730	29.42	0.06	17.45	21 520 823		

a Power consumption for Zambian smelters (Boulamanti and Moya, 2016).

b Botswana Power Corporation energy charge is BWP0.634 per kWh and demand charge is BWP185.6488 per kW. Exchange rate used is BWP1.0 Bz = US\$0.094.

were obtained from web sources (Connelly, 2017) together with spot values for treatment and refining charges for the years 2017 and 2018 (Leung, 2018), which were used to estimate the nominal treatment and refining charges (TR/RC) for the modelled smelter on the KCB. The Foskor chemical plant's product price for sulphuric acid, which is quoted as FCA Richards Bay or exworks, was used as acid buyers from the modelled smelter would similarly collect acid from the site (Foskor, 2018). Commodity price forecasts by the World Bank were used for copper and silver (World Bank, 2018).

# Operating costs – labour and power

The approach adopted in estimating the operating cost is to use the unit costs of a comparable copper smelter in the region. The smelter selected is the Kansanshi copper smelter in Zambia, which is based on the ISASMELT technology and treats copper concentrates to produce copper anodes and sulphuric acid. The labour required to operate the smelter and acid plant complex is assumed to be independent of the capacity, and therefore data from a reference plant can be used, or if this is not available, it can be estimated from the productivity ratio and the anode capacity of the reference copper smelter. Once the number of employees has been estimated, the annual labour cost for the modelled smelter in Botswana is estimated by applying the average monthly wages in the mining and quarrying sector, which is found in the monthly 'Formal Sector Employment Survey' by Statistics Botswana. The estimated labour requirement and annual cost for the smelter and acid plant complex is presented in Table IV.

The annual cost of power is based on the power consumption per ton of copper anode for the reference plant, but taking into account the specific tariffs applicable in Botswana. This is presented in Table V.

# Indicative capital costs of a copper smelter and acid plant complex

The capital costs of recent copper smelter projects were researched from web sources and the six-tenths rule was applied to estimate the capital cost for a given capacity of modelled smelter for the KCB. The Kansanshi copper smelter in the Zambian Copper belt, which was commissioned in 2015 with a smelting capacity of 1.2 Mt/a copper concentrate at 26% copper to produce 300 000 t of copper anodes and 1 Mt sulphuric acid, was used. The 2012 estimates at US\$635 million and US 20 cents per pound were used for the project capital cost and smelter costs respectively (First Quantum Minerals, 2012). More recent web reports indicated that the smelter and acid plant complex was constructed from early 2012 and commissioned in mid-2015 at a cost of US\$900 million. It is also reported that the smelter achieved a quick ramp-up to full production in just over five months (Kansanshi Mining, 2018). According to First Quantum's press release of 12 October 2013, the copper smelter project

capital cost was estimated at US\$690 million, implying that the acid plant capital cost would have been US\$210 million in 2014. The six-tenths rule uses as a reference the copper smelter capital cost of US\$690 million and capacity of 1.2 Mt concentrate per annum, and the sulphuric acid plant's capital cost of US\$210 million for a 1 Mt/a plant, to estimate the cost of an ISASMELT and sulphuric acid plant for the modelled smelter in the KCB. As the estimated capital costs are assumed to be for the year of commissioning, 2014, an escalation factor is applied using the Chemical Engineering Plant Cost Index (CEPCI). Table VI presents the estimated capital costs of the modelled KCB copper smelter and sulphuric acid plant based on a minimum economic size that would provide a real return of 8.0%.

The six-tenths rule is a well-known method for estimating the capital cost of a plant given that of a similar, recently constructed plant using the same technology. The accuracy of such desktop study estimates is -30% to +50%.

$$C_2 = C_1 * \left(\frac{Q_2}{Q_1}\right)^{0.6} * \left(\frac{I_t}{I_0}\right)$$

where

 $C_2$ ,  $Q_2$  = Cost and capacity of plant to be estimated, respectively  $C_1$ ,  $Q_1$  = Cost and capacity of reference plant  $I_t$  = Cost index of the plant in year 2  $I_2$  = Cost index for the reference plant.

# Fiscal regime

In terms of Schedule Twelve of the Income Tax Act of Botswana, a base metal mining project is taxed under a variable rate income tax formula (VRIT) in which the annual rate of tax is computed based on the profitability ratio of the project as follows:

Annual tax rate = 
$$70 - \left(\frac{1500}{X}\right)$$

where X = profitability ratio, defined as taxable income / gross income

The annual tax rate will be not less than the company tax rate, which is currently 22%.

Other key aspects of the mining fiscal regime that would apply to the modelled KCB copper smelter are a 100% accelerated depreciation of capital with unlimited loss carry forward.

# The discounted cash flow financial model

The model determines the minimum economic size of the smelter and sulphuric acid complex using goal seek. Two concentrate sourcing scenarios are modelled to determine the profitability of the smelter complex when treating only local concentrates and when supplementing any spare capacity with imported concentrates. The projected proportions of feed to the smelter are given in Table VII. These two concentrate sourcing scenarios are then evaluated under two fiscal regimes, the variable rate income tax (VRIT), which applies to base metals, and the lower taxation regime that applies to manufacturing businesses. Extending this lower taxation regime to the copper smelter and acid plant complex would improve the project economics for the copper concentrate producers. Other things being equal, this would also lead to higher tax revenue from the mining stage of the copper value chain, which would partly offset the foregone fiscal benefits from a lower tax rate.

The input variables that were used to run a discounted cash flow financial model for the KCB copper smelter and sulphuric acid complex are presented in Table VIII. The values are in constant 2018 money terms. The model assumed an 8% real discount rate based on current mining industry practice.

# Results

The project economics for a copper smelter with a capacity of 485 kt concentrate and 370 kt acid per annum are presented in Table IX. The projected local copper concentrate supply would result in poor project economics, represented by scenario 1. The real NPV (8%) would be a negative US\$144.496 million; IRR would be 3.42%, and the payback period 13 years. These poor project economics would not be enhanced significantly and would fail to turn positive under a low tax scenario, showing just a marginal improvement to NPV (8%) of negative US\$48.471 million: an IRR of 6.5%, and a real payback period of 12 years. Scenario 3 assumes that the smelter would be able to secure additional concentrates from the region, and this is the case that was used to determine the minimum size of the smelter and under the mining fiscal regime with VRIT, it gives an NPV (8%) of zero; an IRR of 8% as expected, and a payback period of 10 years. Scenario 4 assumed that there would be a case for taxing the smelter as a manufacturing business. The real NPV (8%) would be a positive US\$134.712 million; the IRR would be 11.03%, and the payback period 10 years.

# Table VII

Feed profile by source to the KCB smelter

	Proportion of feed to the smelter (%)									
Year	1	2	3	4	5	6	7	8–13	14	15–25
Base case			45	56	56	56	61	80	61	48
Base case	Local		45	56	56	56	61	80	61	48
+ imports	Import		55	44	44	44	39	20	39	52

Table VI									
The estimated capital cost for a copper smelter (minimum economic size) and acid plant in the KCB									
	CEPCI index								
				2014	2018				
Kansanshi smelter	1.2	690	690						
KCB smelter	0.485	401.1	401.1						
Kansanshi acid plant	1.0	210	210	576.10	576.40				
KCB acid plant	0.370	115.8	115.8						

#### Table VIII

### Input variables for the KCB financial model

	Calculation	Amount (US\$ million per annum)
Revenue from treatment charges, free metal, and metal premium	485 000 t conc. × \$161.50 per ton	78.328
Revenue from acid sales	485 000 t conc. × 0.763 t acid per ton conc. × \$118.36 per ton acid	43.800
Total annual revenue		122.128
Annual labour operating costs	600 workers × \$1710.42 per worker × 12 months	12.315
Annual power costs	(see Table V)	21.521
Total annual operating costs		33.836
Earnings before interest, taxes, depreciation and amortization	88.292	
Capital cost of smelter and sulphuric acid plant (assume spent equally over 24 months)	(see Table VI)	516.9
Allowance for maintenance	Assume 1% of capex	5.169

#### Table IX

### Project economics for a 0.485 Mt/a concentrate KCB copper smelter and 0.370 Mt/a sulphuric acid complex

	Project economics in real 2018 money terms (US\$ million)							
Tax and imports scenario	NPV (5%)	NPV (8%)	NPV (10%)	IRR (%)	Payback (years)			
VRIT; no imports	(61.2)	(144.5)	(182.4)	3.42	13			
Low tax; no imports	61.4	(48.5)	(98.2)	6.50	12			
VRIT; with imports	132.4	0	(60.5)	8.00	10			
Low tax; with imports	349.4	134.7	39.0	11.03	10			



The NPV is most sensitive to revenues, followed by capital costs, and is least sensitive to operating costs (see Figure 2).

#### Discussion

The results of the model indicated that for the expanded production cases of the two projects, Cupric Canyon's Khoemacau project or Zone 5, which is at the mine development stage and Tshukudu Metals' T3 project, which is at the full feasibility study stage, the concentrate production is not sufficient to support a copper smelter and sulphuric acid plant for Botswana copper projects. Copper concentrates from these projects are destined for smelting in Chinese smelting and refining complexes, and they have to travel long distances by both land and sea to reach these smelters and refineries. If the full potential of the KCB becomes clearer with more detailed resource delineation that leads to development of more mines or expansion of capacity at

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existing mines, then the outlook for a local copper and sulphuric acid plant would be improved. It is important to realize that the sulphuric acid plant would not only be included to meet the environmental compliance requirements, but also to serve as a source of significant by-product revenues.

One of the factors in the establishment of the copper smelter and sulphuric acid plant would be the level of tax that would apply to it. The smelter and acid plant complex would clearly be a major industrial investment that the policy-maker could use to negotiate a tax agreement, as scenario 4 demonstrated that if the manufacturing tax rate of 15% is applied to the project, this would turn around the project economics from poor to satisfactory with a real NPV (8%) of a positive US\$134.712 million; an IRR of 11.03%, and a real payback period of 10 years. The potential benefits of taxing the smelter as a manufacturing business include the following.

- There would be an improvement in the net smelter returns to local producers of concentrate, which will not only enhance their profitability but also the life of their projects due to the increase in reserves that would result from reduced cut-off grades.
- There would be an improvement in tax revenues at the mining stage, which will slightly offset the foregone tax revenues from the copper smelter being taxed at a lower rate than the producers of copper concentrates.
- The production of sulphuric acid would provide the key ingredient in the production of fertilizers.
- Finally, the local production of acid would create opportunities for the exploitation of oxide and supergene copper sulphide ores through leaching, solvent extraction, and electrowinning, a process that is characterized by lower capital and operating costs than the pyrometallurgical route.

The economic viability of the copper smelter complex would also be driven by the electricity tariffs, as these have been found to make up approximately 30–35% of the operating costs (Boulamanti and Moya, 2016). The Botswana Power Corporation is currently expanding its grid into the KCB and there is therefore an expectation that tariffs will continue to rise, which would erode the project economics unless the smelter could negotiate sustainable rates for its business.

# Conclusion

The purpose of this study was to establish whether the projected tonnage of locally produced copper concentrates from Mowana copper mine and from projects at advanced stages in exploration and mine development in the Kalahari Copper Belt of Botswana would justify the establishment of a copper smelter and a sulphuric acid plant in the KCB. The Kansanshi copper smelter and sulphuric acid plant near Solwezi, in Zambia, which employs the ISASMELT smelting technology and was commissioned in 2015 at an estimated capital cost of US\$900 million, was used as a reference project for the capital cost estimates for both the copper smelter and the acid plant. This study concluded that the projected tonnage of copper concentrates production in Botswana would not justify the establishment of a smelter and acid plant on its own, and that a lower tax rate would vastly improve the project economics. There are other studies that would need to be carried out at a greater level of detail at the prefeasibility stage to further understand the viability of this project. These include:

- Further investigations into the ability of the copper projects under development to increase their total production to about 0.5 Mt of concentrate per annum
- A study of the likelihood of concentrate imports from existing or planned projects in the region to augment local concentrate production so that the copper smelter can be operated at near full capacity of 0.5 Mt/a concentrate
- A market study to establish the likely revenue and offtake quantities of sulphuric acid, as revenue from the sale of acid is significant in the smelter project economics,
- Initial discussion with the Botswana government regarding a tax agreement for the project to pay tax at the rate for manufacturing businesses, which is currently set at 15%
- A preliminary investigation into whether the power parastatal would be in a position to negotiate charges for power that would not hurt the sustainability of this project.

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